

34<sup>th</sup> JSMCWM annual meeting &  
3RINC's Autumn

# Hydrogen production from Organic waste using reforming reaction







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Waste to Hydrogen Laboratory  
based on Smart Process Analysis

- I Introduction
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# Introduction



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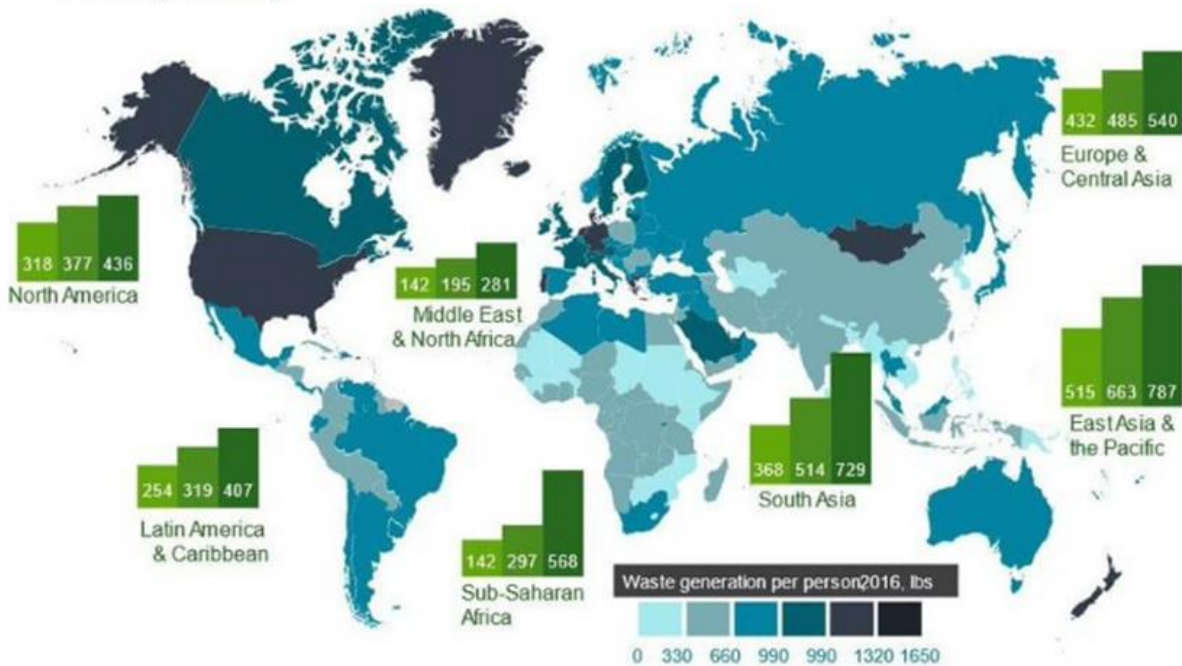




## A THROWAWAY WORLD

Regional waste generation  
US ton (millions)

2016 2030 forecast 2050 forecast



### Increase of waste

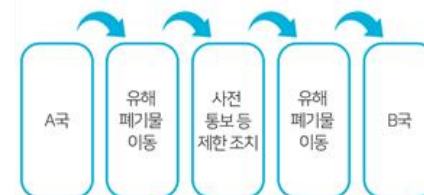


### Ocean disposal X

생활폐기물 매립지 사용 만료 전망



### Lack of landfill



### Limitation of waste trade

폐기물의 기존 처리 방법 (해양투기, 매립, 소각 등)을 대체할 수 있는 전략 마련의 필요성이 증대됨



# Carbon neutrality, Net Zero

Net zero means that CO<sub>2</sub> emissions due to the human activity are in balance with global absorption, so that the concentration of CO<sub>2</sub> in the atmosphere does not increase further

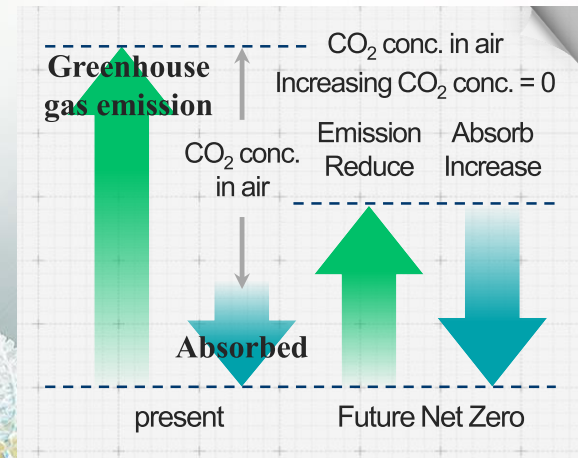
It is necessary to reduce anthropogenic emissions of CO<sub>2</sub> and increase the amount of absorption (removal) using forest restoration and negative emission technology\*

Amount of Carbon emission =  
Absorb or removal amount of Carbon  
Substantial Carbon emission  
will be 'Zero'



Carbon emission

Absorbed Carbon



1.5 °C

To become within 1.5 °C of increasing average temperature

**Necessity of Net Zero 2050**



11<sup>th</sup>

Greenhouse gas emission in Korea (2018)

**11<sup>th</sup>**  
(\*Among the OECD 5<sup>th</sup>)



134 Countries

After Paris agreement (2015), Net Zero declaration

**By 134 countries**  
(Sep. 2021)



40 %

Korea set 2030 greenhouse gas reduction compared to 2018

**26.3% to 40%**

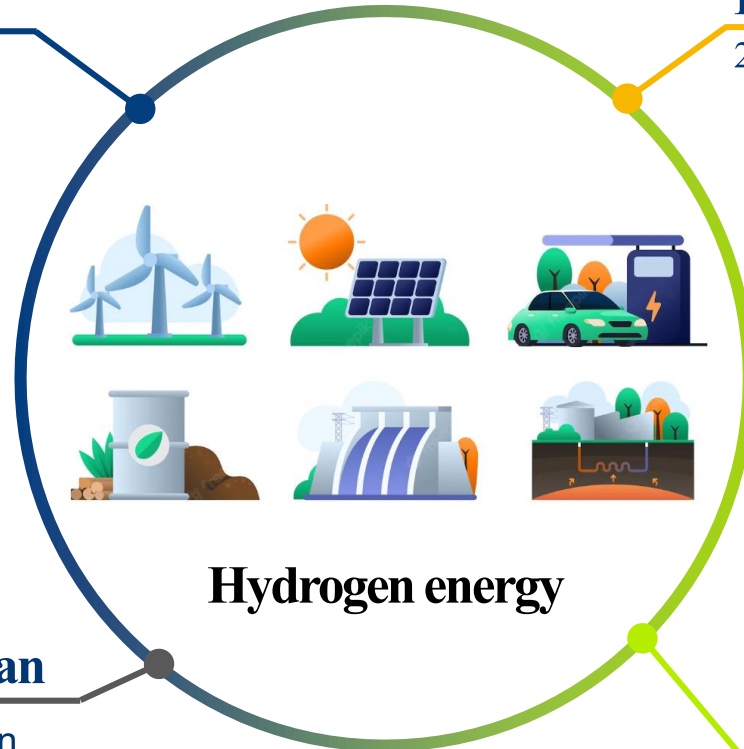


## Alternative energy

The way to replace fossil fuels

## High energy efficiency

2~3 times higher than thermal engine



Hydrogen energy

## Eco-friendly and clean

Less greenhouse gas emission and pollutants

## Sustainable energy

Unlimited amount energy source comparing to fossil fuels

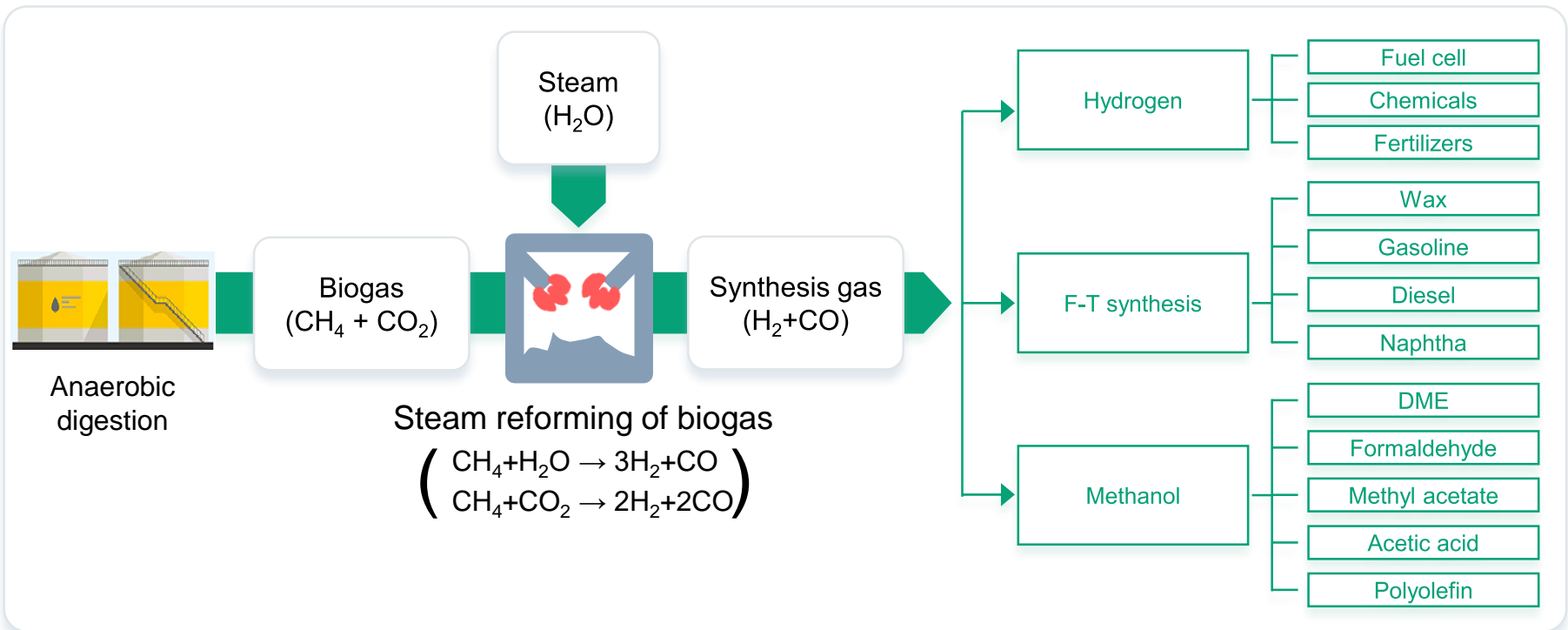


# Organic waste to hydrogen

## Steam reforming of biogas

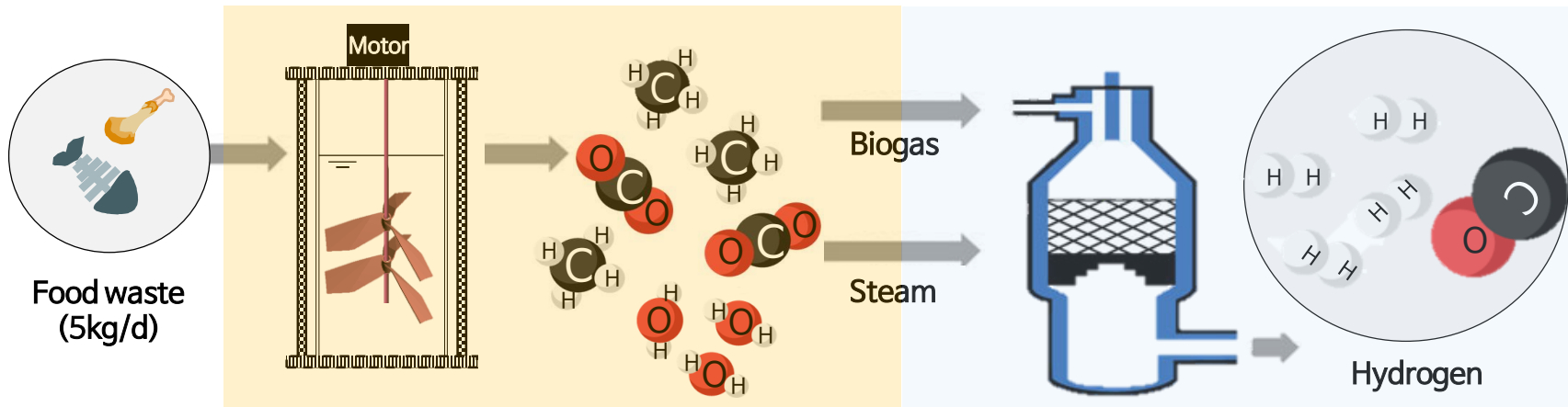
Hydrogen production from biogas generated from organic waste  
(Converting  $\text{CH}_4$  and  $\text{CO}_2$  into  $\text{H}_2$  and  $\text{CO}$  through reforming of biogas with steam)

Steam reforming of biogas | Instead of combustion of biogas to produce heat





# Research goal



## Biogas & H<sub>2</sub> production

**01** Optimization of anaerobic digestion



**Optimization of digester**

**02** Optimization of reforming



**Optimization of reaction condition & Development reforming catalyst**

**The development of system for organic waste to hydrogen is required**





# Research 1. Anaerobic digestion

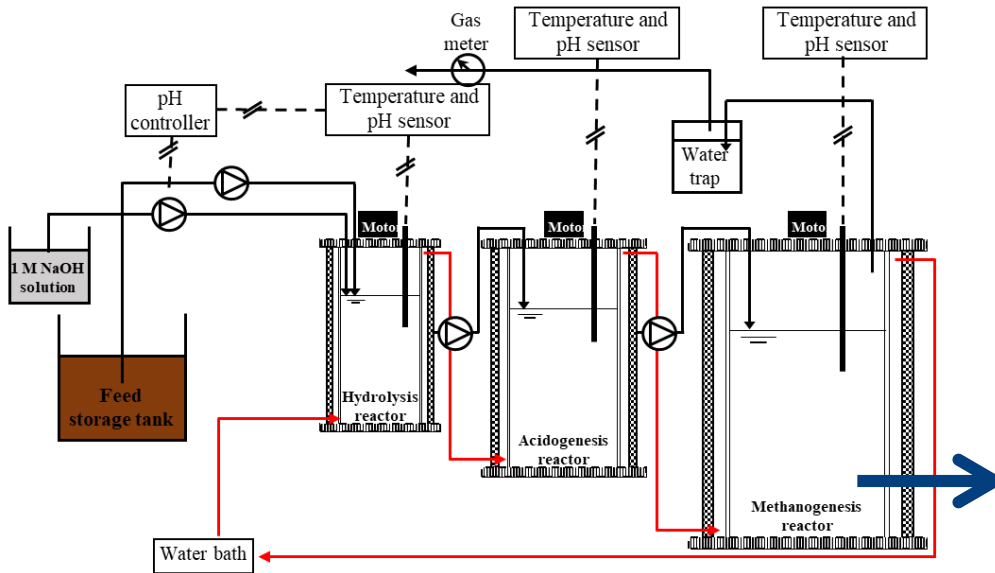


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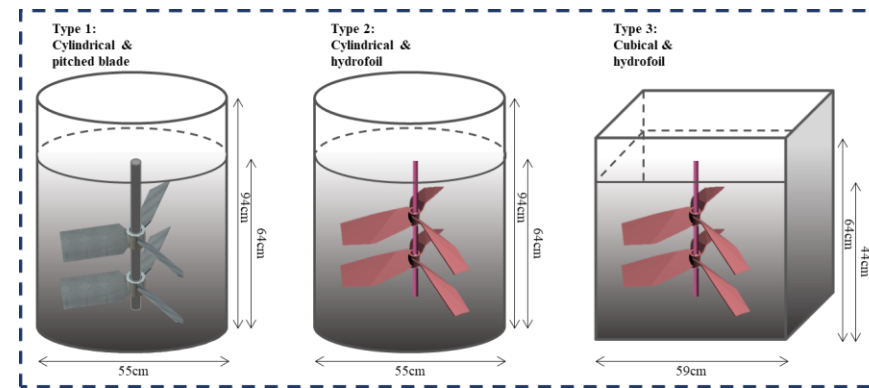


# Optimization of Anaerobic digestion

## ❖ Anaerobic digester



## Type of reactor and agitator

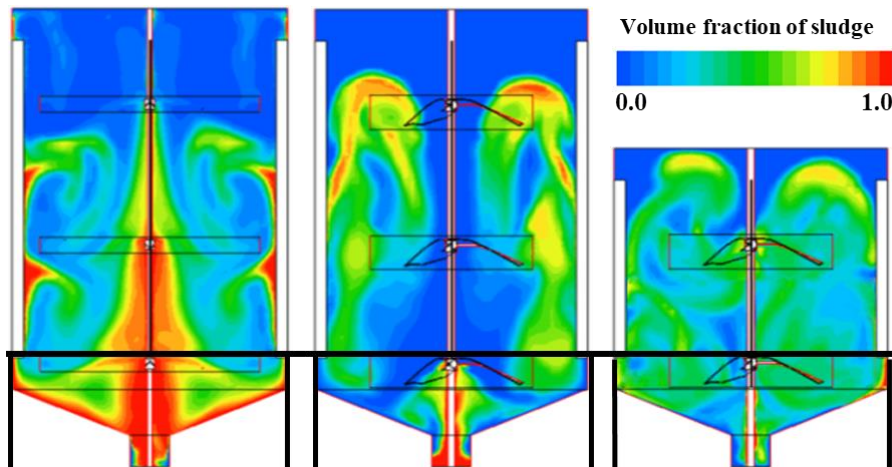




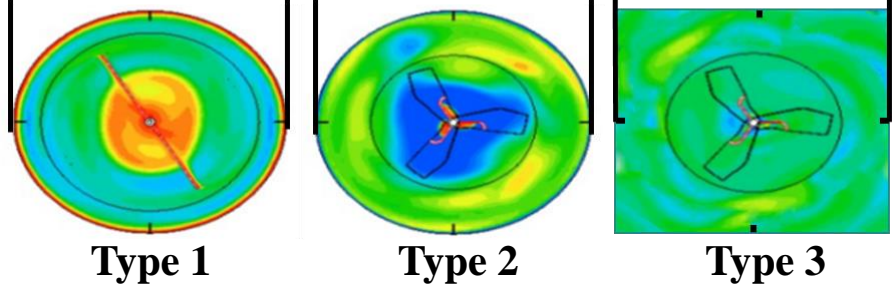
# Simulation results (computational fluid dynamics)

Volume fractions of sludge with different type of reactor obtained by CFD

(a) Front view



(b) Top view



- Highly dispersed volume fractions of sludge is resulting from better mixing efficiency
- Type 3 reactor showed the highest distribution of volume fraction due to the axial flow caused by Hydrofoil agitator and enhanced turbulence flow in edges of cubical reactor.





## Pollutant removal efficiencies and biogas production

Indicator	Type 1	Type 2	Type 3
	Cylindrical shape Pitched blade	Cylindrical shape Hydrofoil	Cubical shape Hydrofoil
Removal efficiency	TCOD (%)	65.8	76.5
	TS (%)	62.1	72.2
	VS (%)	62.2	72.4
Biogas production	Biogas yield (L/kg FW*)	72.3	84.1
	Methane yield (L/kg FW)	42.1	51.3
	Methane content (%)	58.2	61.3

- A comparison of types 1 and 2 showed that hydrofoil agitator exhibited a higher removal efficiency and biogas production due to the axial flow caused by the hydrofoil agitator
- A comparison of types 2 and 3 revealed that the cubical reactor enhanced the COD, TS, and VS removal efficiencies and biogas production, which resulted from the turbulence flow



## Research 2. Reforming of biogas



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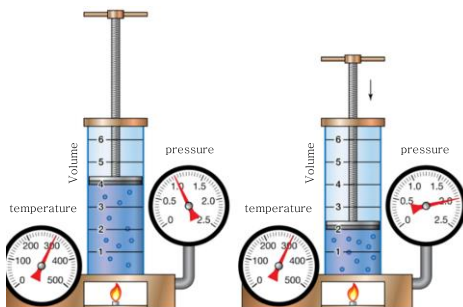
# Optimization of reforming of methane

## Parameters

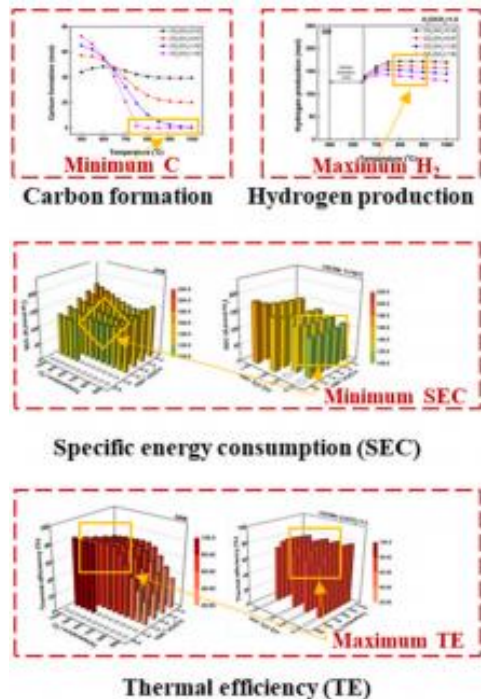
Reaction temperature

Oxidant/ $\text{CH}_4$  ratio

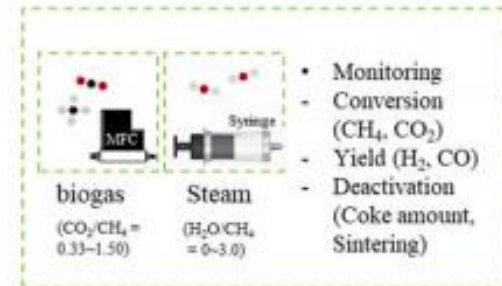
Oxidant type



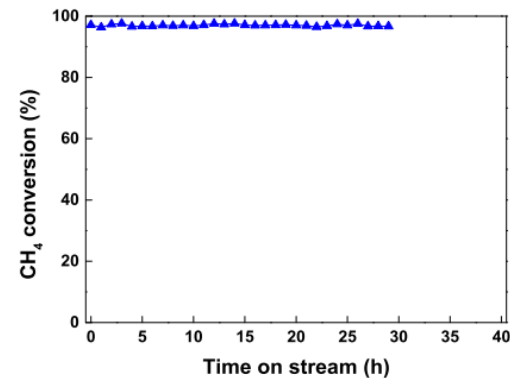
## Simulation



## Validation



### Reforming reaction



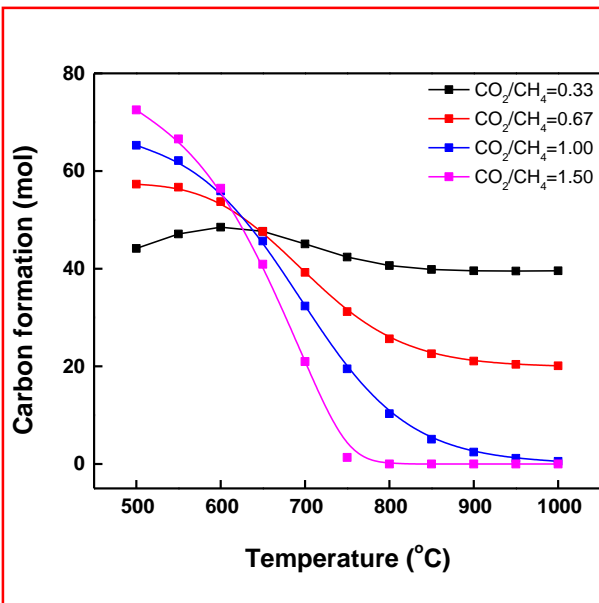




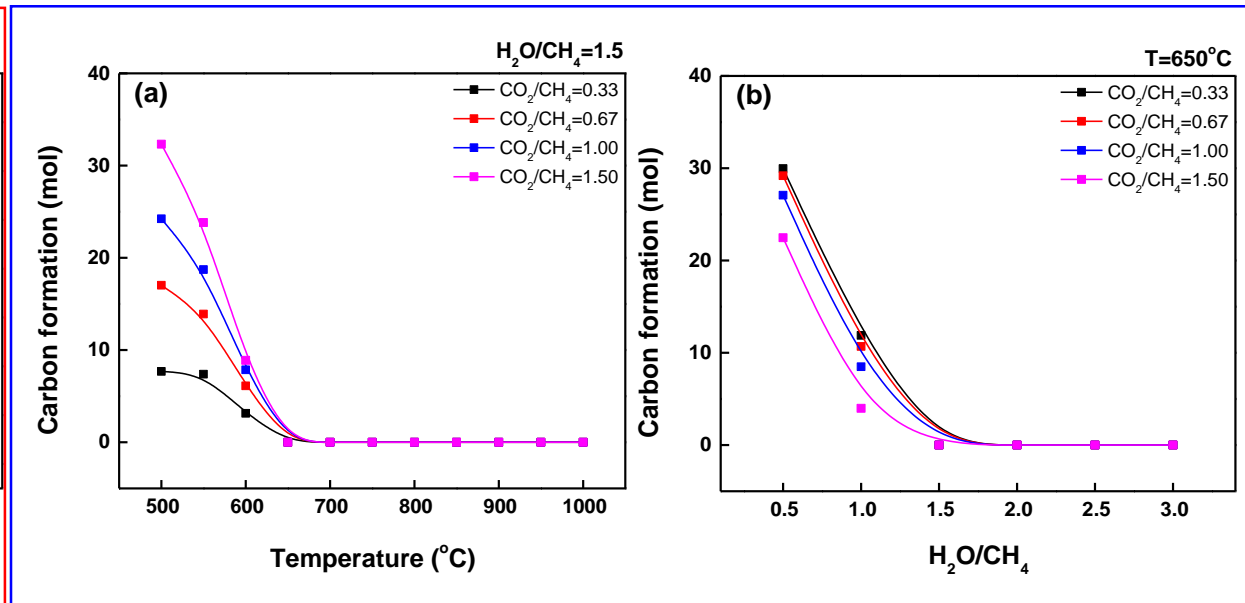
# Simulation results (optimization of oxidant)

## The relationship between oxidant and carbon formation

### Biogas reforming



### Biogas steam reforming



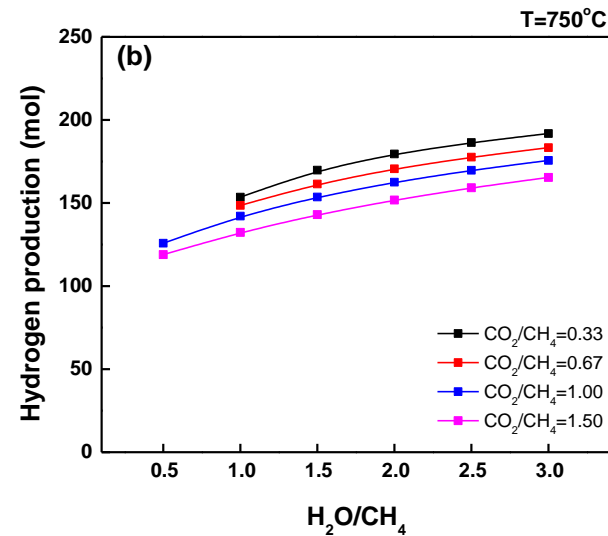
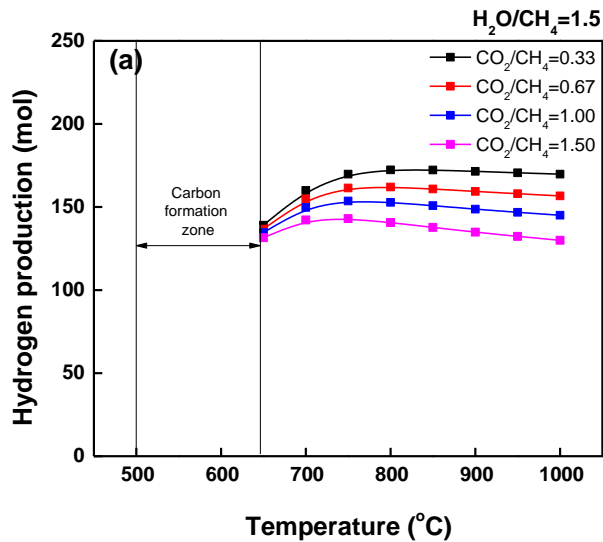
➤ In biogas reforming, carbon formation can be suppressed by maintaining a reaction temperature of  $> 800$  °C and a  $\text{CO}_2/\text{CH}_4$  ratio of  $> 1.50$ .

➤ In biogas steam reforming,  $\text{H}_2\text{O}/\text{CH}_4$  ratio  $> 1.5$  and temperature  $> 650$  °C were required to prevent the carbon formation.



# Simulation results (Reaction conditions and H<sub>2</sub> production)

## The relationship between reaction conditions and hydrogen production

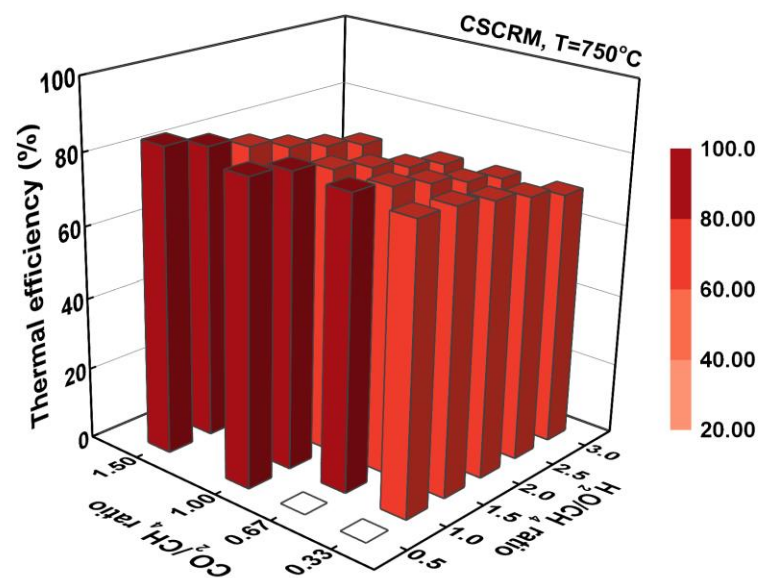
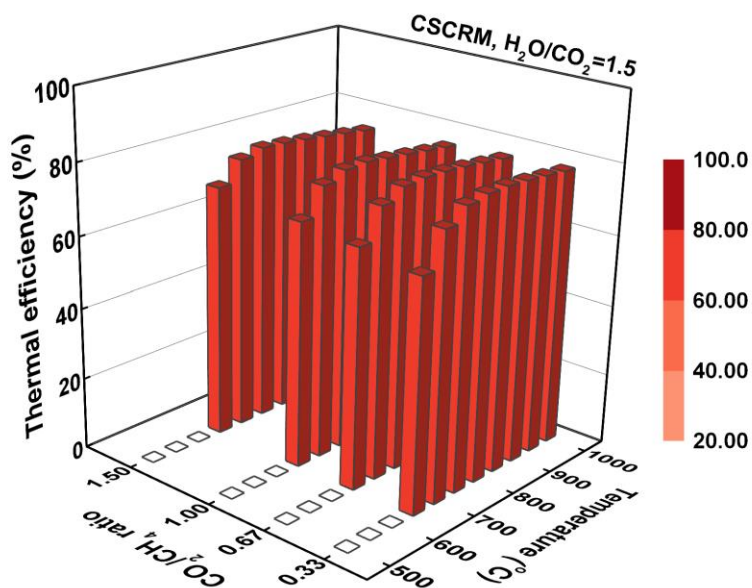


- H<sub>2</sub> production increased up to 750 °C and decreased thereafter, regardless of the biogas composition
- Hydrogen production increase with increasing steam/CH<sub>4</sub> ratio and increasing CH<sub>4</sub> content in biogas



# Simulation results (Reaction conditions and H<sub>2</sub> production)

The relationship between reaction conditions and thermal efficiencies



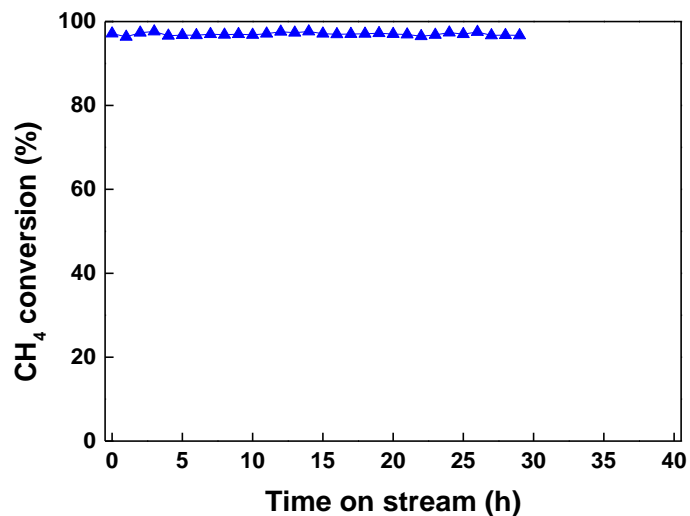
- At > 800 °C, thermal efficiency decreased with increasing temperature; thus, 750 °C was the optimal temperature for the steam reforming of biogas.
- Although a high thermal efficiency was achieved at a low H<sub>2</sub>O/CH<sub>4</sub> ratio. However, low H<sub>2</sub>O/CH<sub>4</sub> ratio causes carbon formation, the optimum ratio was fixed at 1.5.





# Validation results

## The catalyst activity test and deactivation study



Catalyst	Coke (g/g <sub>cat</sub> )	Ni crystallite size (nm)	
		Reduced	Used
Ni-MgO-CeZrO <sub>2</sub>	0	11.33	15.19 (34%)

- CH<sub>4</sub> conversion over the Ni-MgO-CeZrO<sub>2</sub> catalyst was maintained for 30 h without a significant decrease, indicating that the optimized reaction conditions were energy effective and favored stable H<sub>2</sub> production in the real biogas steam reforming reaction.
- No carbon was deposited on the catalyst during biogas reforming under optimized conditions.
- Ni crystallite size slightly increased but it was not affect to deactivation of catalyst.

# IV

## Future research plans



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# Demonstration project for hydrogen production



## Scale up

### Process scale up

- Catalyst production scale
- Plant scale

## Data acquisition

### Biogas data

- Composition
- Impurities

## Scenario study

### Techno environ. Analysis

- Economic efficiency
- Environmental impact



# 감사합니다.

