



Suitable flocculant selection and continuous wastewater treatment using Mg-Al layered double hydroxides - a case study targeting mine wastewater containing As and Fe

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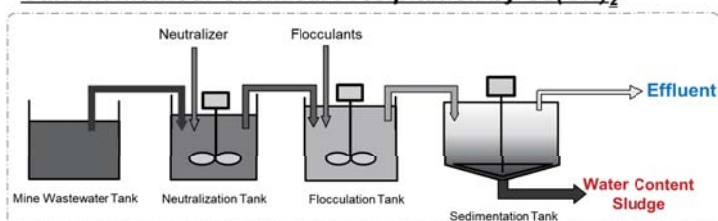
Introduction - Mine wastewater treatment

Mine Wastewater

- Highly acid
- Toxic heavy metals
- Harmful to humans and environment

Treatment to meet effluent standard is vitally necessary

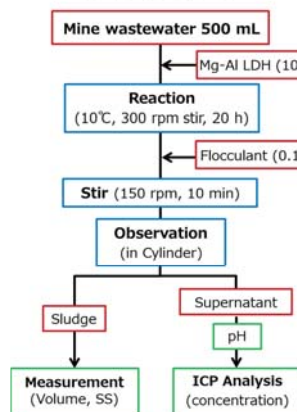
Current method: Chemical Precipitation by Ca(OH)₂



- ▲ High water-content sludge generated
- Enormous energy and high costs to manage
- Shortage in intermediate/final disposal sites

Suitable flocculant selection for LDH Treatment [2]

Experimental



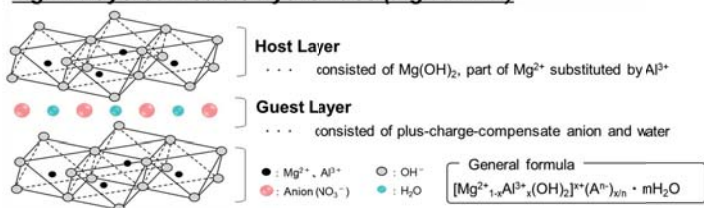
Post-treated water quality

	LDH only	LDH+ A100	LDH+ A110	LDH+ A175
pH [-]	6.78	7.35	7.03	7.43
Sludge [mL]	16	16	20	28
SS [mg/L]	25	9.0	6.5	6.3
Fe [mg/L]	0.080	0.10	0.036	0.26
As [mg/L]	n.d.	n.d.	n.d.	n.d.

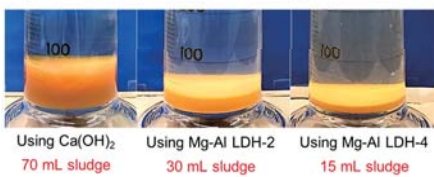
- Combination of flocculant reduced SS.
- Water quality parameters all cleared standard.
- ACCOFLOC®-A110 selected as suitable flocculant.

Introduction - treatment by Mg-Al LDH

Mg-Al Layered Double Hydroxides (Mg-Al LDH)



Our earlier study [1]: treating mine wastewater 500 mL



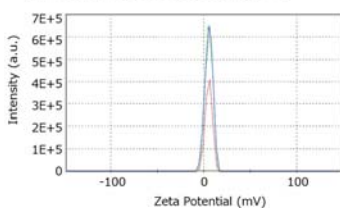
- As, Fe concentration, pH, SS all met Japanese Effluent Standards
- Treatment by LDH reduced sludge volume to a large extent

Objective of this study

- Suitable flocculant selection for LDH treatment
- Continuous treatment operation and cost analysis

Suitable flocculant selection for LDH Treatment [2]

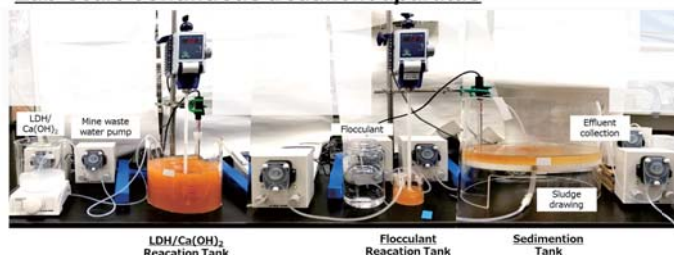
Flocculant candidates



Basic Structure in common (Polyacrylamide)		
Type	Ionicity	Solution pH
ACCOFLOC®-A-100	Weak-anionic	6 ~ 8
ACCOFLOC®-A-110	Medium-anionic	6 ~ 8
ACCOFLOC®-A-175	Strong-anionic	7 ~ 9

Continuous treatment and cost calculation [2]

Lab-scale continuous treatment apparatus



Calculation equation

$$\text{Agent cost} = \text{Annual mine wastewater throughput} [\text{m}^3/\text{year}] \times [\text{JPY}/\text{year}] \quad [\text{LDHs}/\text{Ca}(\text{OH})_2 \text{ unit price} [\text{JPY}/\text{ton}] \times \text{dosage} [\text{ton}/\text{m}^3] + \text{flocculant unit price} [\text{JPY}/\text{ton}] \times \text{dosage} [\text{ton}/\text{m}^3]]$$

$$\text{Sludge transportation cost} = \text{Annual mine wastewater throughput} [\text{m}^3/\text{year}] \times \text{Sludge volume} [\text{m}^3/\text{m}^3] \times \text{transportation unit price} [\text{JPY}/\text{m}^3]$$

Comparison between treatment using LDH and using Ca(OH)₂

	Using LDH	Using Ca(OH) ₂
Agent Dosage	LDH/Ca(OH) ₂ [ton/m ³] 7.8 × 10 ⁻³	1.2 × 10 ⁻³
	ACCOFLOC®-A-110 [ton/m ³] 1.6 × 10 ⁻⁶	2.0 × 10 ⁻⁷
Water Quality	As, Fe concentration	Complies with Japanese Standard
	SS [mg/L] 3.3	5.3
	pH [-] 6.49	7.51
Sludge	Final volume [mL/L] 40.3	68.2
	Water content [%] 58.9	84.7
Cost	LDH/Ca(OH) ₂ unit price [JPY/ton] 150,000	40,300
	Agent cost [JPY/year] 2,284,342,285	97,888,795
	Sludge transportation cost [JPY/year] 144,754,267	244,711,913
	Total cost [JPY/year] 2,429,096,551	342,600,708

- Treatment using LDH: less sludge, lower water content, cut transportation cost

Conclusion

- Combination of ACCOFLOC®-A-110 reduced SS after treatment
- Treatment by LDH generate less sludge and low water content ⇒ landfill and energy saving
- Treatment by LDH could save sludge transportation cost up to 40%
- Lower unit price of LDH (< 12,819 JPY/ton) is expected ⇒ lower agent cost

[1] X. Yang, M.T. Rahman, T. Kameda, Y. Masaki, Y. Saito, S. Kumagai, T. Yoshioka, *Mine Water and the Environment.*, DOI:10.1007/s10230-020-00697-4, 2020.

[2] X. Yang, H. Osawa, T. Kameda, Y. Masaki, Y. Saito, S. Kumagai, T. Yoshioka, *International Journal of Environmental Science and Technology*, 2020 (under review).